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## **Chemical oxygen demand oxidation via sustained-release persulfate balls: a rate-compatibility study of flow velocity, releasing, and oxidation**

### **Key words:**

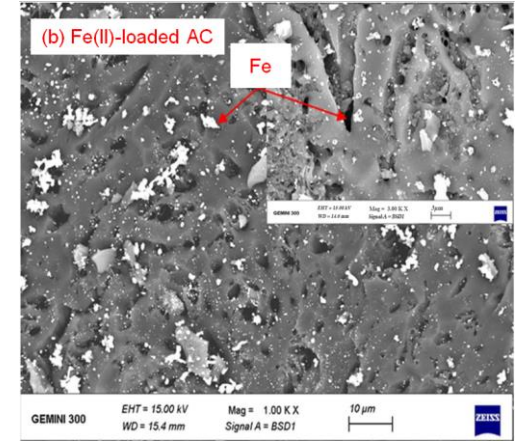
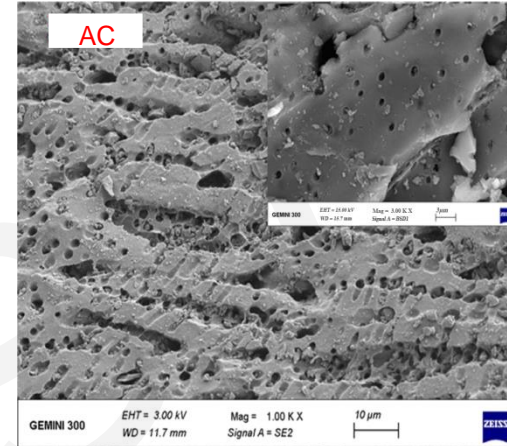
Chemical oxygen demand (COD); Sodium persulfate (PS); Sustained-release balls;  
Permeable reactive barrier (PRB); Fe(II)-loaded activated carbon (Fe-AC)

## Introduction

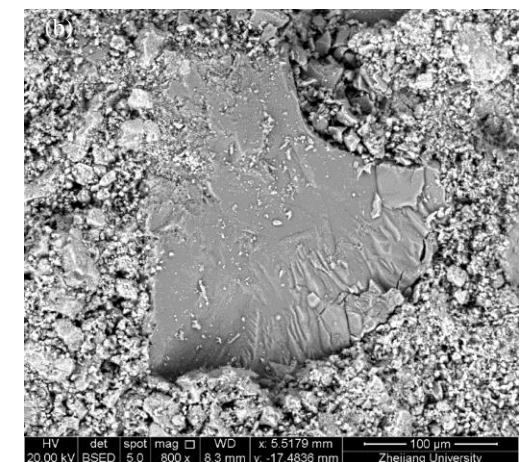
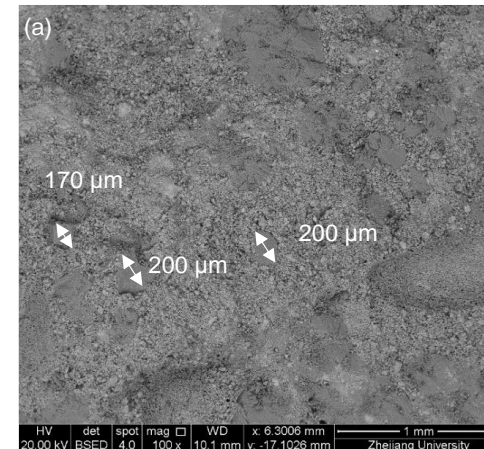
- ❑ Site removal of organic contaminants (chemical oxygen demand, or **COD**) from municipal solid wastes (MSW) by permeable reactive barrier (**PRB**) is popular
- ❑ Oxidation by **sustained-release persulfate (PS) balls** is adopted
- ❑ Release rate of PS balls, a function of **ball diameter**, should match chemical kinetics for maximal efficiency
- ❑ The compatibility of **flow velocity**, **oxidant-releasing rate** and **oxidation rates** is challenging

# Materials

- Sustained-release persulfate balls, with weight ratio of **10.7:0.24:1.4:1** (**PS:cement:sand:water**), was manufactured
- COD removal rate maximal at **95%**
- SEM images of AC, Fe-AC revealed that **crystals of Fe(II) occupied and clogged AC micropores**
- PS ball diameter between **170 and 200  $\mu\text{m}$**  in the sustained-release balls



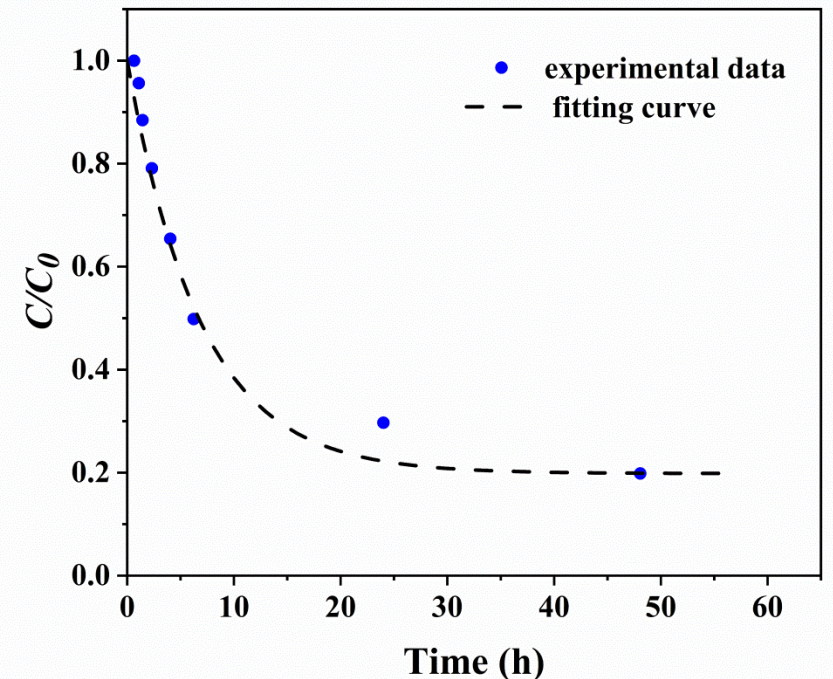
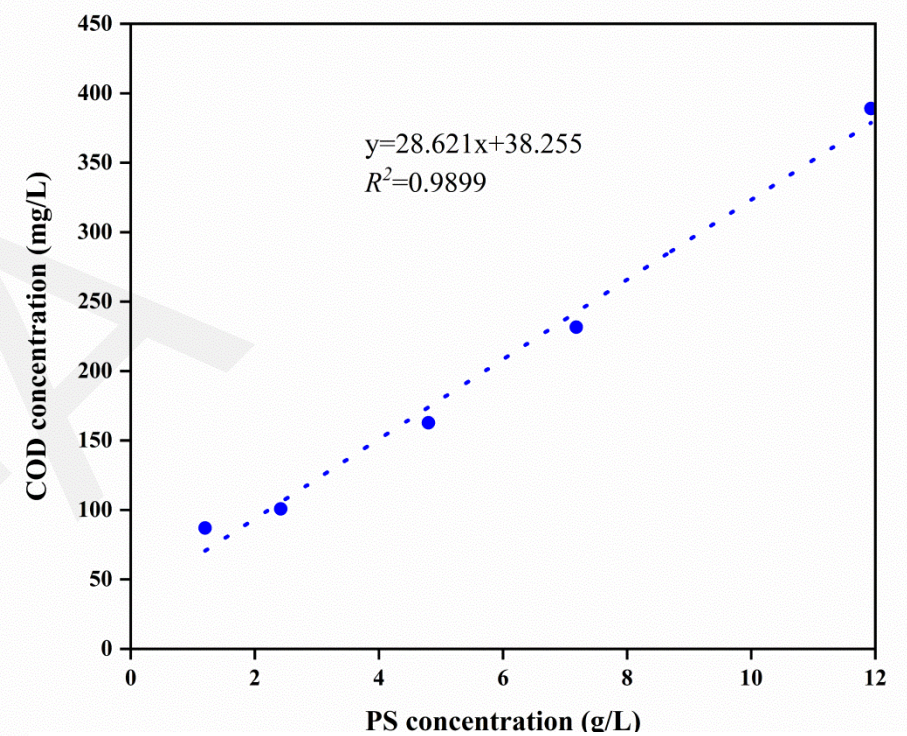
SEM images of AC before and after Fe(II) loading



SEM images of sustained-release PS balls

# COD Oxidation Kinetics

- $\text{Cr}_2\text{O}_7^{2-} + 3\text{S}_2\text{O}_8^{2-} + 2\text{H}^+ \rightarrow 2\text{Cr}^{3+} + 6\text{SO}_4^{2-} + \text{H}_2\text{O} + 3\text{O}_2$ .
- COD removal by Fe-AC-catalyzed PS
- **First-order** kinetic reaction assumption
  - $K$  is  $0.83 \text{ h}^{-1}$
  - $t_{0.5}$  is  $0.83 \text{ h}$
- COD removal by Fe-AC-catalyzed 4 pebbles of sustained-release PS balls
- **Pseudo-first-order** kinetic reaction assumption
  - $K$  is  $0.15\text{h}^{-1}$
  - $t_{0.5}$  is  $4.62 \text{ h}$



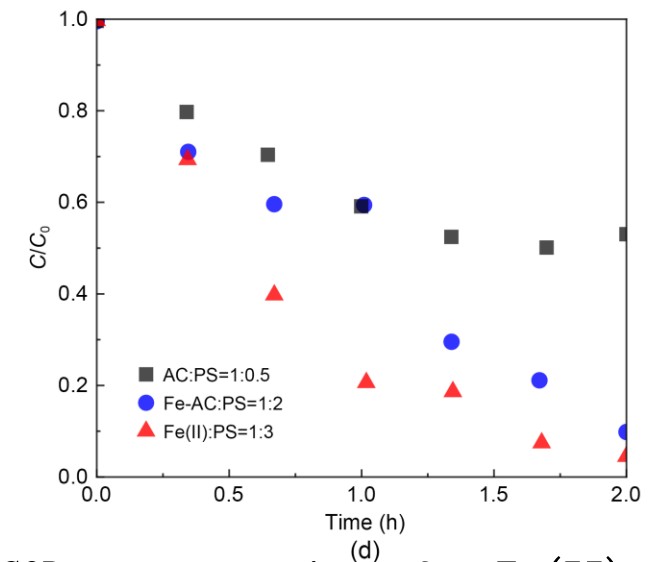
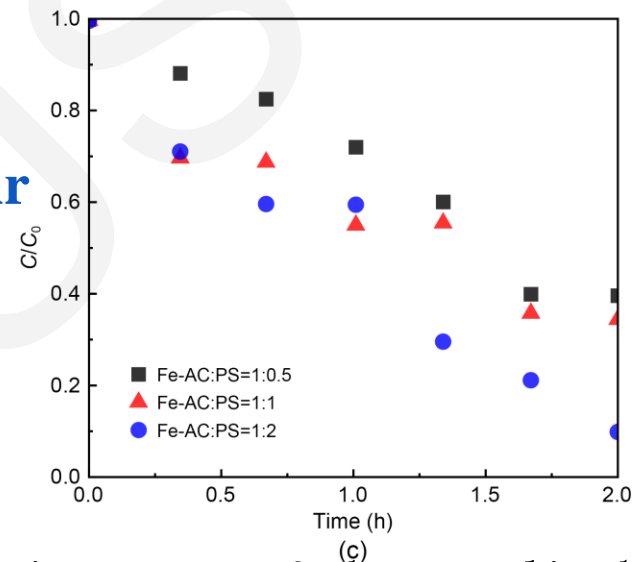
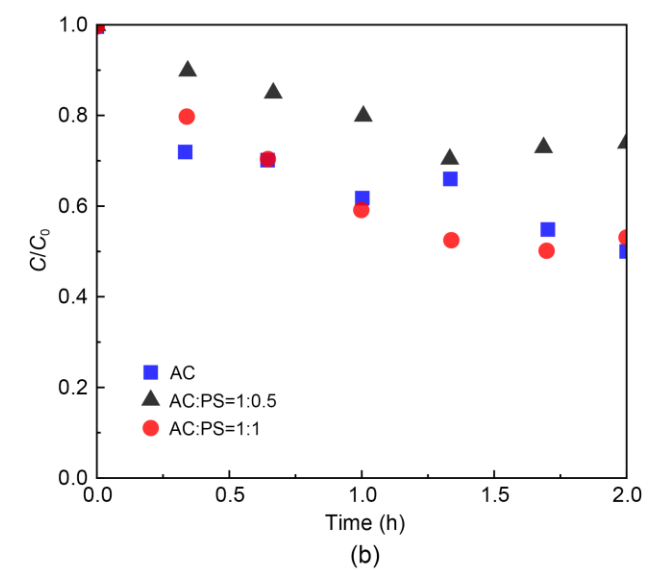
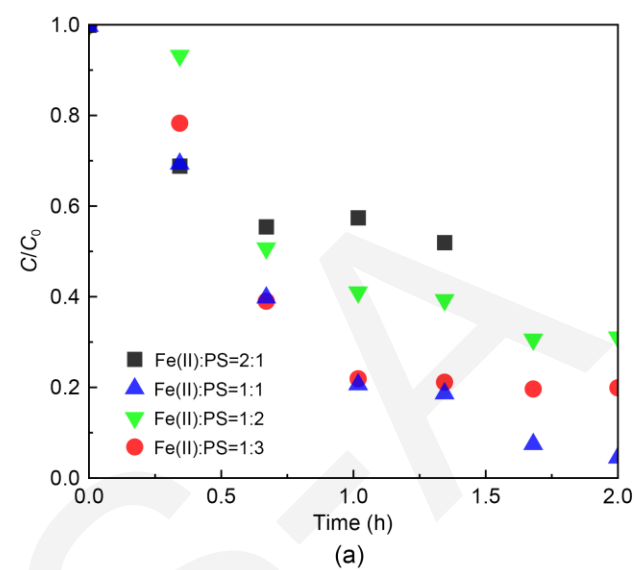
# COD removal efficiency

Fe(II):PS = 1:2, COD removal rate was 95%

Catalysis of PS by Fe-AC impressive COD

removal rate of up to 90%

- $S_2O_8^{2-}$ :12COD ratio was 1.02
- $Fe^{2+}$  easily oxidizing in the presence of air



Time-evolution curves of the normalized COD concentrations for Fe(II) (ferrous sulfate) and PS at different ratios (a), AC and PS at different ratios (b), Fe-AC and PS at different ratios (c), and AC and PS, Fe-AC and PS, as well as Fe(II) and PS at a certain ratio (d)

## COD removal efficiency

- Linear relationship between the ball diameter  $D$  (mm) and half-life period

- $t_{0.5} = 0.060D + 0.215$

- The ball diameter and kinetic rate constant of PS release ( $k$ )

- $k = 544.6/D$

Release rates of the sustained-release PS balls

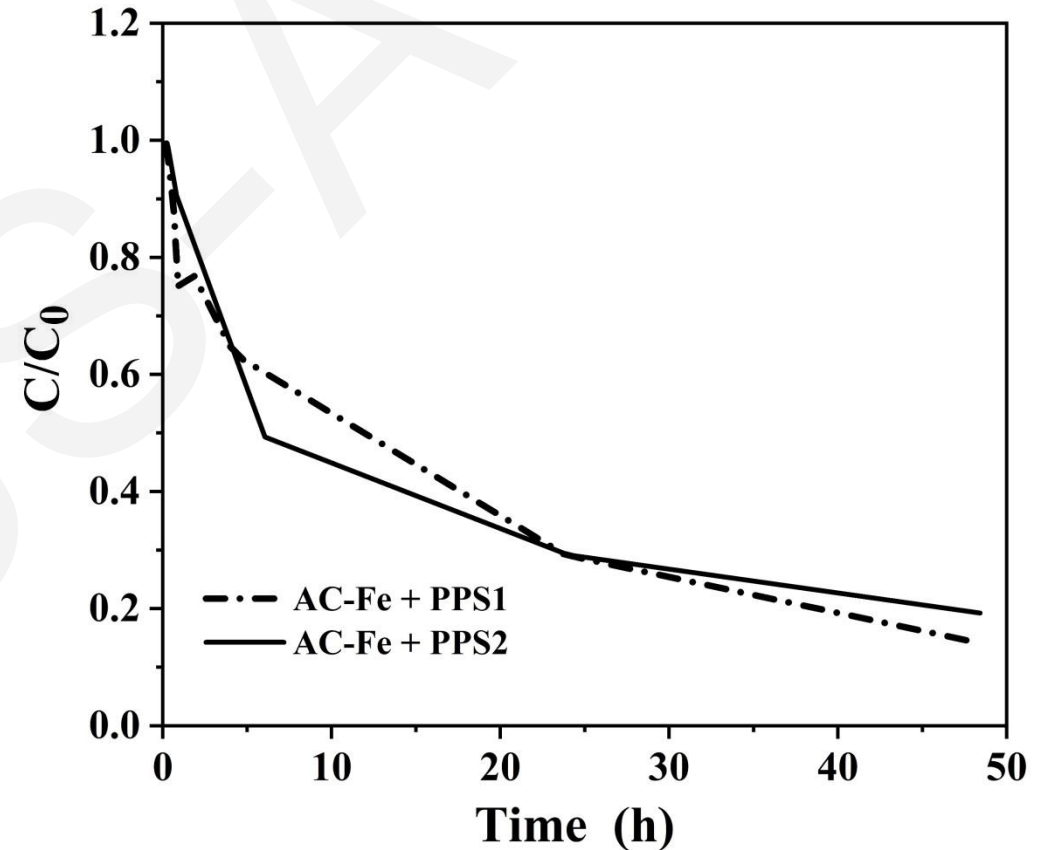
Particle size (mm)	Fitting curve	Release rate (mg/(g·d))	$t_{0.5}$ (d)
5	$q_1 = 7098t / (63.14 + 112.27t)$	112.27	0.56
10	$q_2 = 4370t / (55.23 + 79.14t)$	79.14	0.70
15	$q_3 = 1064t / (35.92 + 29.60t)$	29.60	1.21
20	$q_4 = 778t / (32.91 + 23.63t)$	23.63	1.39

Sustained-release ball parameters for different sizes

Ball diameter (mm)	$q_{max}$ (mg/g)	K (mg/(g·d))	SSE	$R^2$
5	63.14	112.27	14.61	0.9879
10	55.23	79.14	16.77	0.9873
15	35.92	29.60	15.82	0.9779
20	32.91	23.63	8.05	0.9872

## Compatibility between the PRB flow rate and the PS release rate

- $aAV_0C_0 \leq \frac{A}{D^2Mk} \times 10^6$
- Column test
- COD concentration = 200 mg/L
- maximum flow rate in the PRB = 0.21 m/d

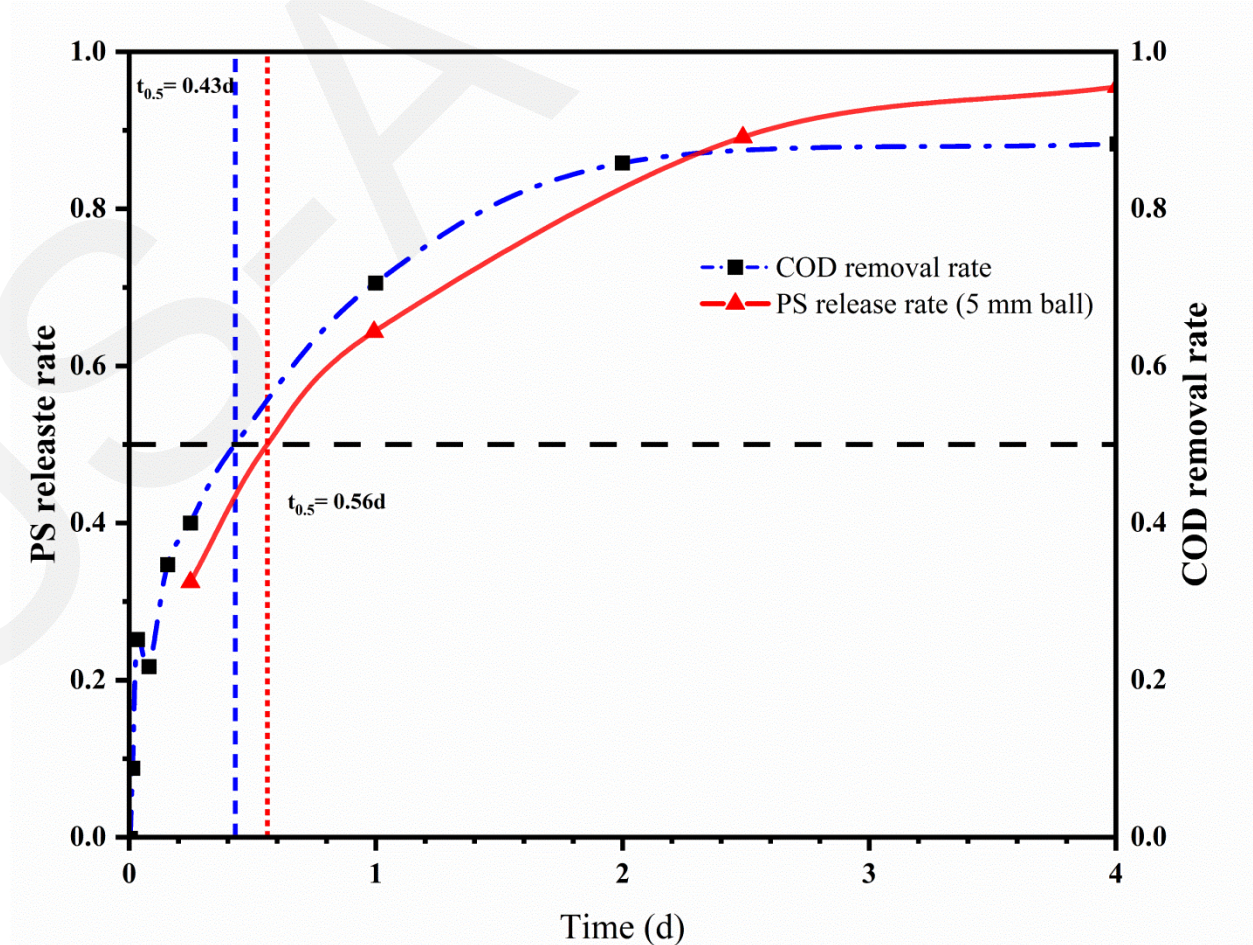


Removal effect of COD with an oxidizing filler by using Fe-AC with two pebbles (PPS1) and four pebbles (PPS2) of sustained-release PS balls

# Compatibility of the PS release rate and COD oxidation rate

□  $R_{\text{COD}} = k \cdot \frac{\partial C_{\text{COD}}}{\partial t}$

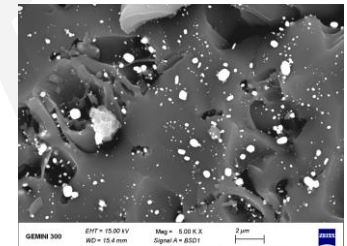
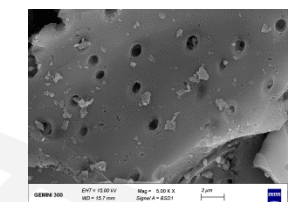
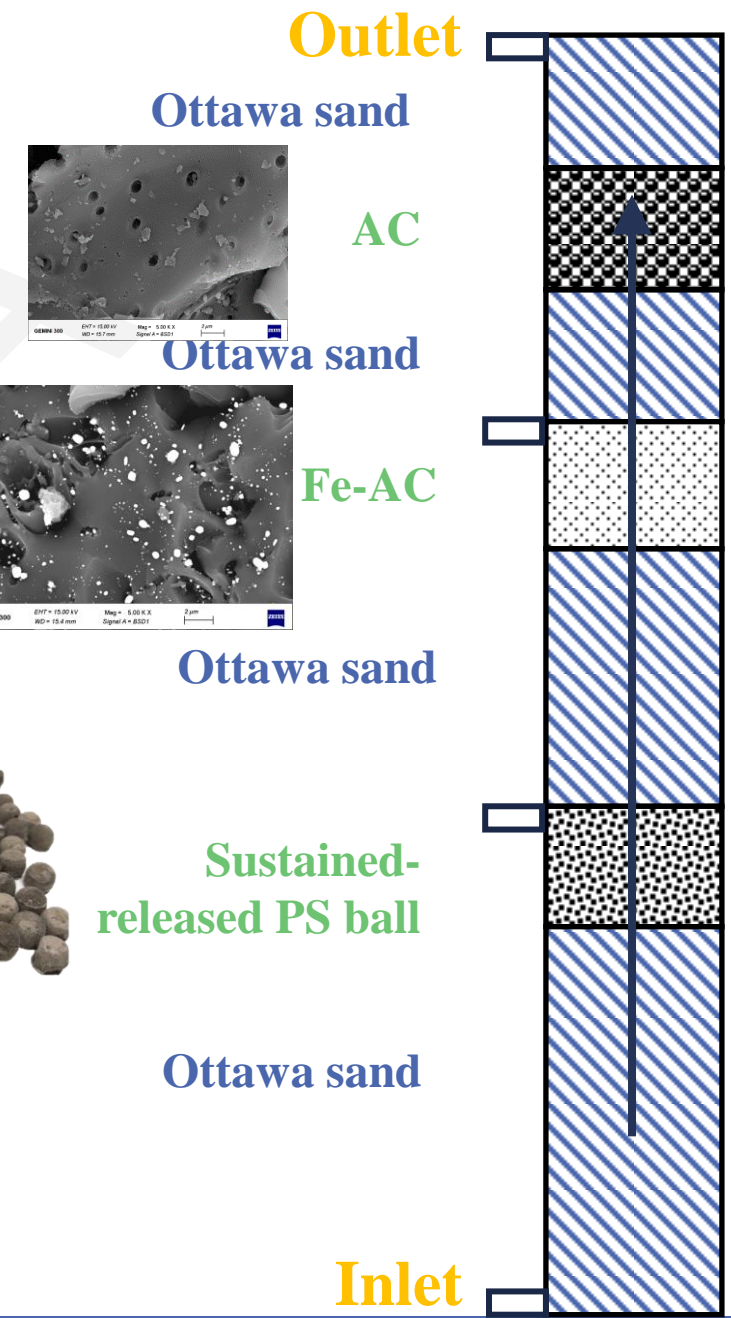
- **Oxidation reaction half-life (0.43 d) close to PS release half-life (0.56 d) of a 5 mm ball**



Kinetic chemical reaction results of Fe-AC-catalyzed sustained-release PS balls that oxidize COD

# Simulation of PRB serviceability

- $$\frac{C_f}{C_0} = \frac{1}{2} \operatorname{erfc} \left( \frac{R_d L - V_s t_b}{2\sqrt{D_h R_d t_b}} \right) \frac{1}{2} \exp \left( \frac{V_s L}{D_h} \right) \operatorname{erfc} \left( \frac{R_d L + V_s t_b}{2\sqrt{D_h R_d t_b}} \right)$$
- $V_0 = 0.21 \text{ m/d}$
- $R_d = 1.27$
- $L = 3 \text{ m}$  (thickness of the PRB)
- Service life of this PRB with a breakthrough threshold of 10% is two years



## Conclusions

- An investigation of the COD oxidation by persulfate sustained-release balls in a PRB setup carried out
- the highest COD removal rate of 95% obtained at optimum dosage ratios of Fe-AC:PS balls and initial PS:COD ratio (12:1 and 12.24:1)
- Sustained-release PS ball diameter of 5mm is compatible with COD oxidation rate
- COD oxidation rate ( $t_{0.5}=0.43$  d) compatible with the 5 mm PS balls release rate ( $t_{0.5}=0.56$  d)